COSMHYC Final Event

24th of February 2021

WELCOME







Program

PART 1

- I. H2 compression: what is at stake? FCH JU, Pietro Caloprisco
- II. The hybrid COSMHYC compression principle & challenges EIFER, Coordinator: David Colomar
- III. The COSMHYC Video

PART 2

- I. Optimized mechanical compressor prototype NEL, Mikael Sloth
- II. Building up a metal hydride compressor prototype EIFER, Rami Chahrouri MAHYTEC, Mathilde Bangoura & Jean-Michel Tisserand
- III. Q&A session 1

PART 3

- I. Testing and results EIFER, Coordinator: David Colomar
- II. Techno-economic assessment LBST, Jan Zerhusen
- III. Q&A session 2







24.02.2021 I COSMHYC Final Event

COSMHYC - Bringing hydrogen compression to the next level





Stay in touch!

COSMHYC project

David Colomar (Project Coordinator)

www.cosmhyc.eu

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@COSMHYC_FCH



COSMHYC and COSMHYC XL









H2 compression: What is at stake?

FCH JU

Pietro Caloprisco

COSMHYC final event

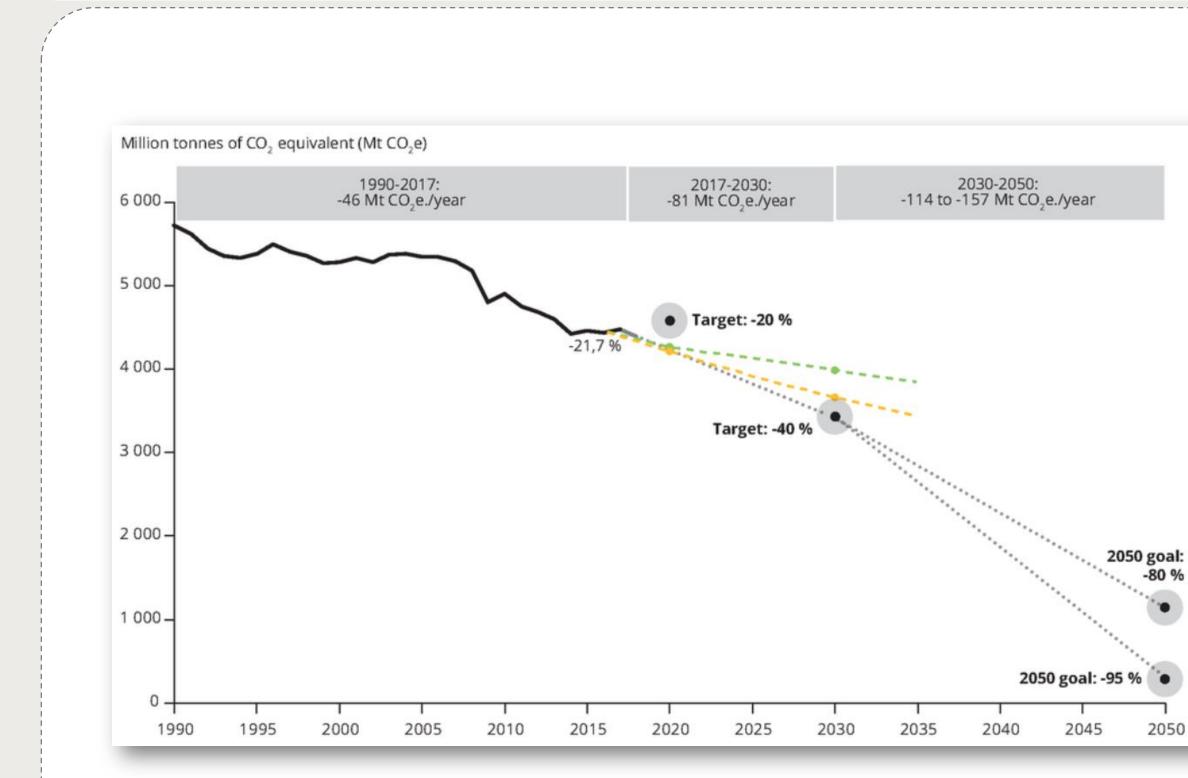


FUEL CELLS AND HYDROGEN JOINT UNDERTAKING



EU CO2 emissions

Stepping up the decarbonisation efforts



Source EEA Dec 2019







- 20% GHG emissions
- + 20% Renewable Energy
- +20 % Energy efficiency

EU 2030 climate & energy targets:

- 40% GHG emissions
- + 32% Renewable Energy
- +32.5 % Energy efficiency



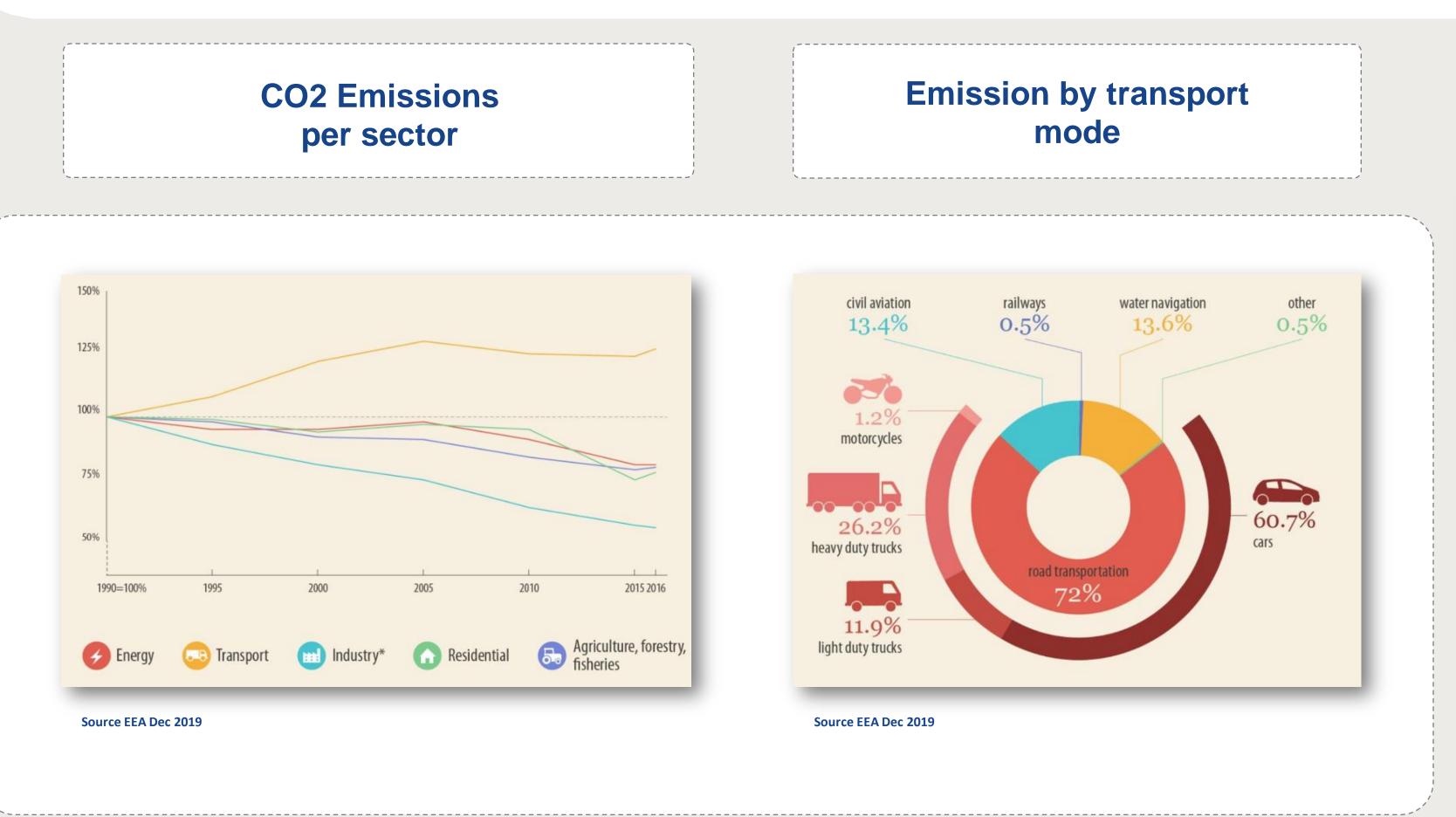
EU Green Deal & other com. -55% GHG emissions by 2030 0% Net GHG emissions by 2050 Transport -90% GHG by 2050





Focus on transport

All transport modes under pressure







ZEV to be introduced in all transport modes

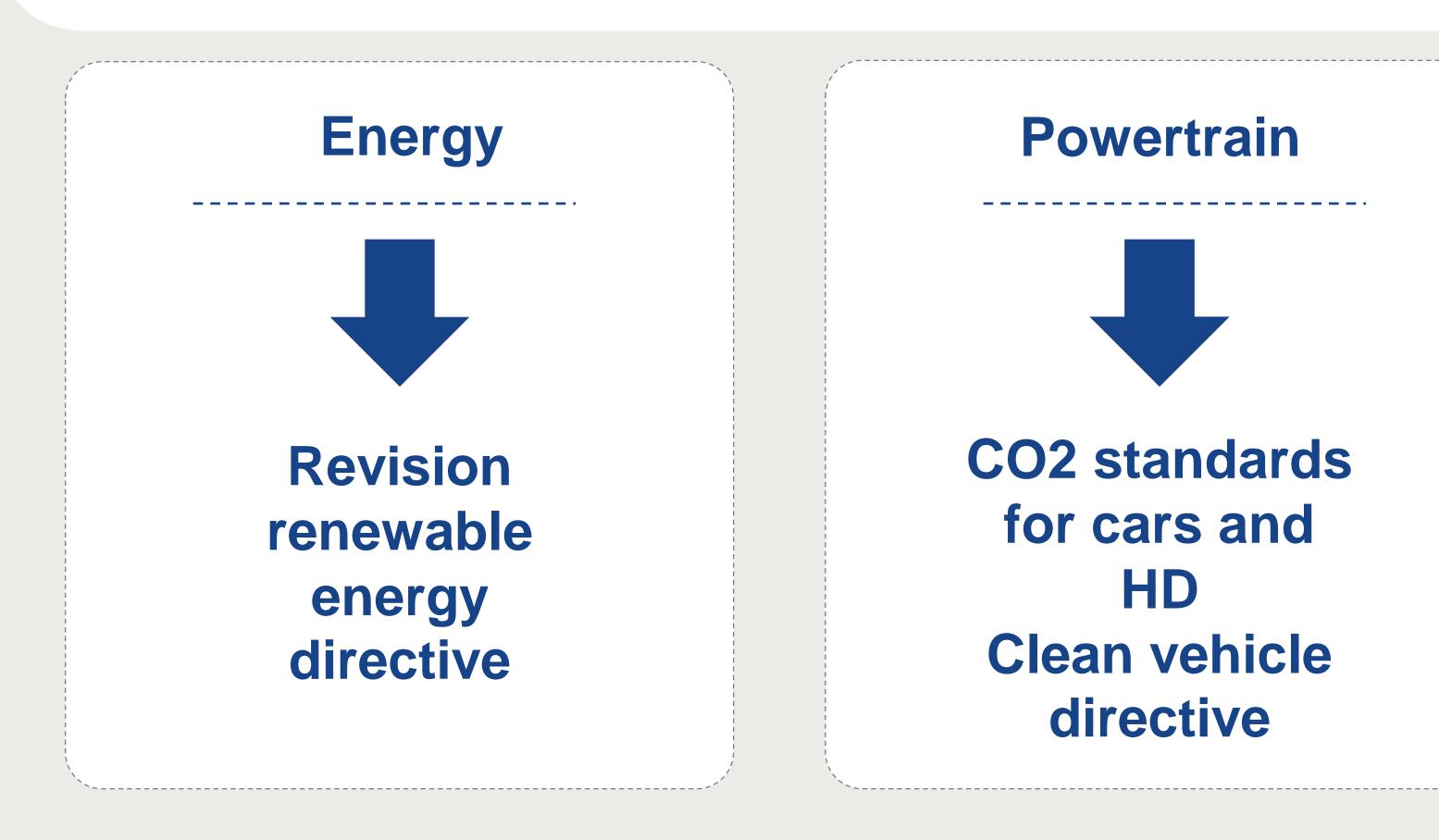






Supporting ZEVs deployment

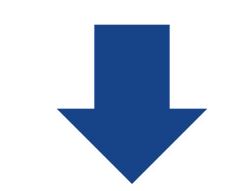
A coordinated approach







Infrastructure



Revision of the Alternative **Fuels** Infrastructure Directive

...and more

R&I: FCH JU





Main themes

Old & new priorities





Compression development remains central





Areas of action

Priorities identified in the SRIA by HE/HER

Early Stage Research Actions (TRL 2-3)

- Efficiency;
- Footprint;
- Noise;
- Cost;
- V2infrastructure communication;

Development Research Actions (TRL 3-5)

- high throughput stations;
- Innovative components to reduce costs;



1. -50% cost HRS;

2.99% reliability



Demonstration Actions (TRL 5-7)

- Standardisation & manufacturability components
- Reliability & safety;
- New business models;

Application Flagship (TRL 7-8)

encourage HRS operators to invest in hydrogen technology and help creating initial networks;

2030

3. HRS network sustaining HD fleet







Thanks for your attention

Pietro Caloprisco

Project Officer <u>Pietro.caloprisco@fch.europa.eu</u>

For futher information

www.fch.europa.eu www.hydrogeneurope.eu www.nerghy.eu



FUEL CELLS AND HYDROGEN JOINT UNDERTAKING





24th of February 2021

The hybrid COSMHYC compression: principle & challenges

Speaker David Colomar EIFER



- eifer

Innovative compression solutions for efficient hydrogen mobility



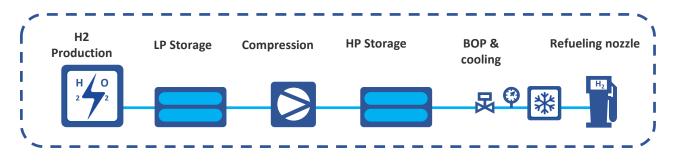


H2 compression, the other bottleneck of the green H2 value chain

Unloading zone Compression HP Storage BOP & Refueling nozzle cooling

Hydrogen refueling station

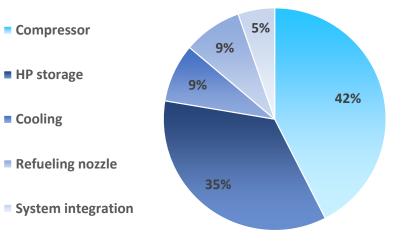
Hydrogen refueling station with onsite production







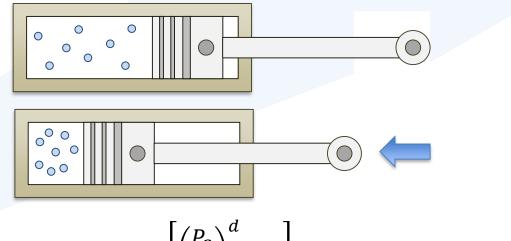
EXAMPLE OF HRS CAPEX DISTRIBUTION







The state-of-the art: mechanical compression



$$W_t = C \cdot T_1 \cdot \left[\left(\frac{P_2}{P_1} \right)^2 - 1 \right]$$

- \Rightarrow Electricity consumption
- \Rightarrow Maintenance, wear and tear
- \Rightarrow Noise disturbance
- \Rightarrow Flow rate & energy depend on inlet pressure

The techno-economic constraints are strongly related to the mechanical nature of the compression





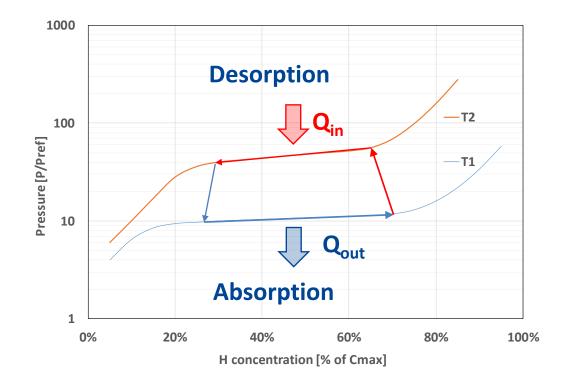
Metal hydride compression: a possible game changer

- ⇒ Principle: an absorption/desorption effect within a metal alloy
- \Rightarrow A heat driven process
- ⇒ A correlation between temperature and pressure

 $M(s) + x/2 H_2 \xrightarrow{absorption} MH_x(s) + Heat$ desorption

 $\ln P_{eq} = \frac{\Delta H}{RT} - \frac{\Delta S}{R}$

Van't Hoff equation:







Metal hydride compression: a possible game changer

- \Rightarrow The core of the reactor: metal hydrides
- ⇒ No more mechanical effect: no moving part, no wear and tear, etc.

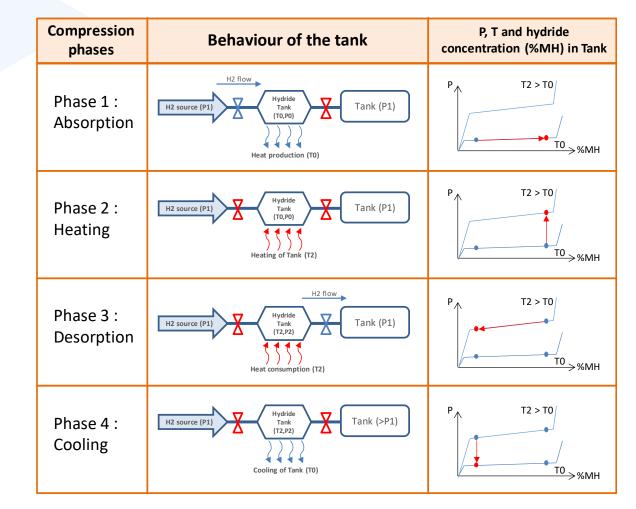








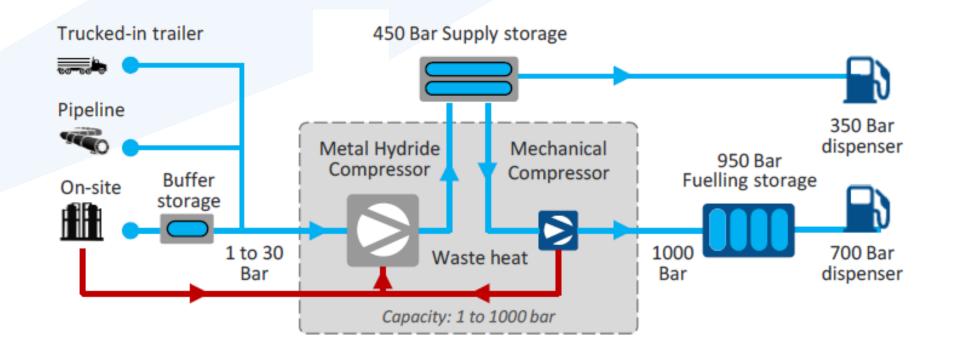








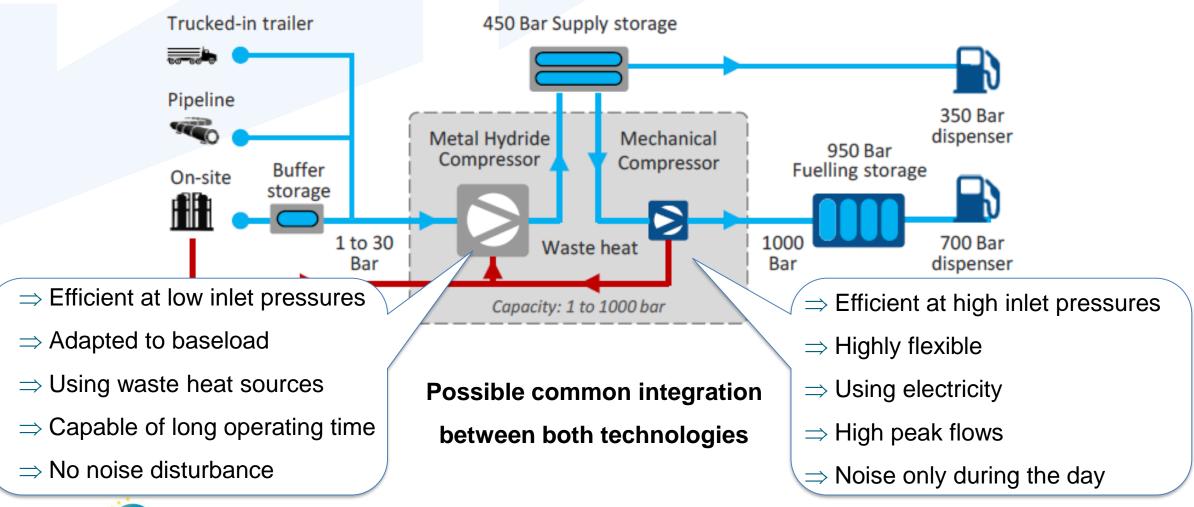
The COSMHYC concept: looking for the best of both technologies







The COSMHYC concept: looking for the best of both technologies

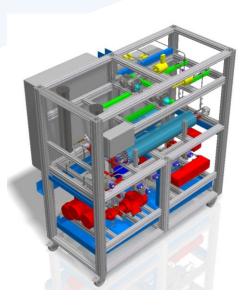


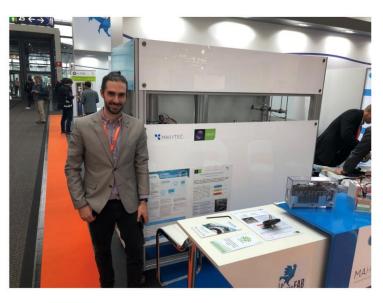


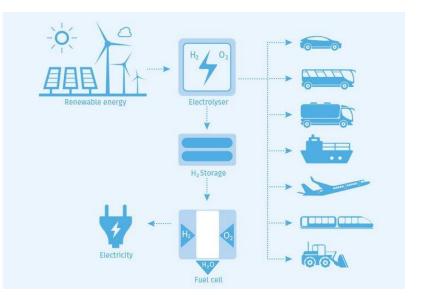


Challenges to meet

- ⇒ Getting rid of rare earths: problem of costs & independence
- ⇒ Defining the right product for the right application: P & T optimization
- \Rightarrow Scaling up: from 1 Nm3/h to > 100 Nm3/h







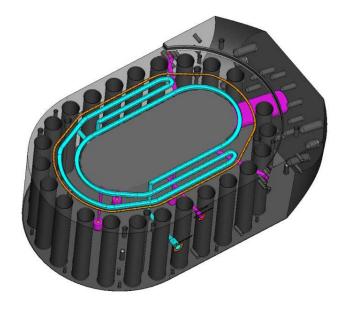


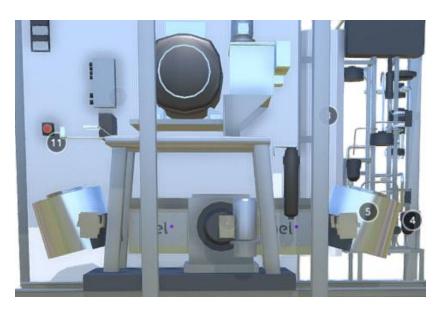


Challenges to meet

- \Rightarrow Improving mechanical compression:
- ⇒ Increasing life time, optimizing design, reducing noise level
- ⇒ Reducing energy consumption and production costs







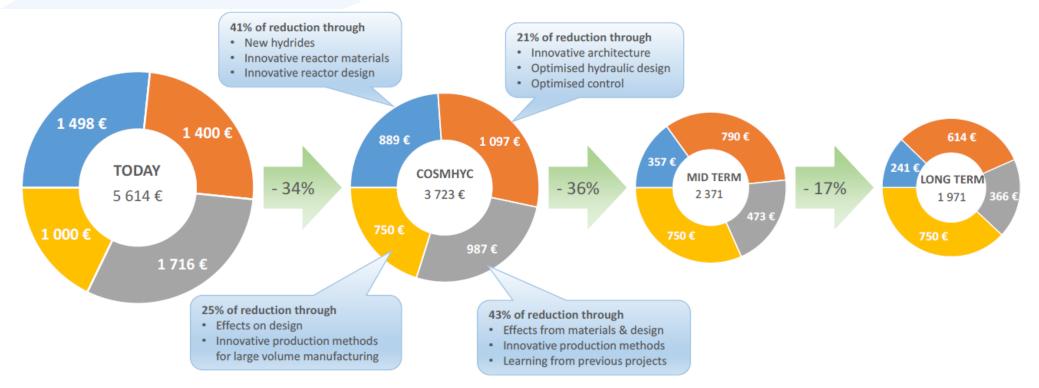




Challenges to meet

 \Rightarrow Increase the level of TRL from 3 to 5 to prepare market introduction

 \Rightarrow Divide by 2 production costs compared to the state-of-the art



Materials costs of the core technology
System integration, auxililiaries & control

Production costs (factory, energy, man power, overheads)
Mechanical compressor





The COSMHYC consortium

- \Rightarrow 5 partners from 3 countries
- \Rightarrow Industry, R&D and consultants





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ludwig bölkow systemtechnik

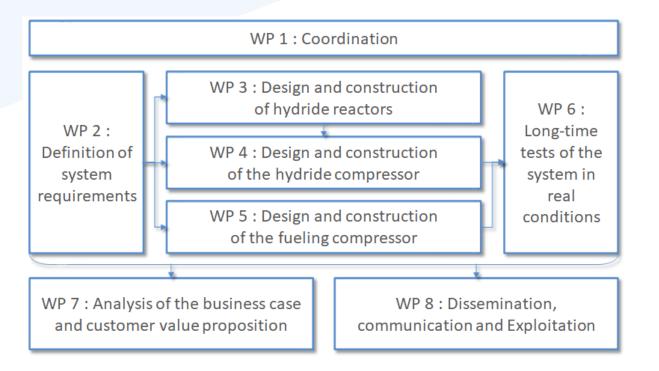
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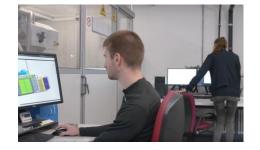




The COSMHYC work plan

- \Rightarrow 4 years of intensive activities
- ⇒ Research, Development, Lab & field tests
- ⇒ Techno-economic analysis, communication, dissemination, exploitation















Thank you for your attention !

Contact: colomar@eifer.org







24th of February 2021

Optimized mechanical compressor prototype

Speaker Mikael Sloth Nel Hydrogen



nel.

Innovative compression solutions for efficient hydrogen mobility





Objectives – Mechanical Compressor (MC)

Objective has been to improve state-of-the-art mechanical diaphragm compression technology (MCH on a range of parameters through R&D, achieving the following targets:

Targets

5% efficiency improvement from 1,25 kWh/kg to 1,18 kWh/kg for 450bar inlet & 1000 bar outlet

Improve diaphragm lifetime from 50 million to 100 million cycles

Reduce noise level from 85dB to <60dB at 5 meters

-25% cost reduction for a manufacturing volume of 50 units from €140/kg to €105/kg at peak capacity of 60kg/h

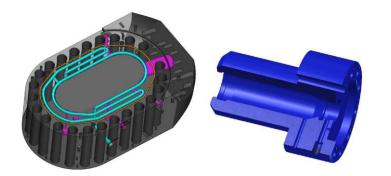




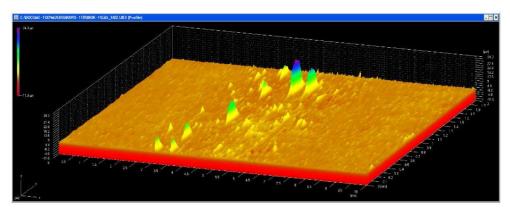
Development – Mechanical Compressor

Key development efforts

- Advanced CFD and FEA models of the MC used for developing and optimizing component designs
- Applying of internal cooling to compressor head and piston rod seal house, to reduce wear
- Improved materials and surfaces for diaphragm in order to increase lifetime (# of cycles)



Internal cooling of components



Diaphragm surface profile

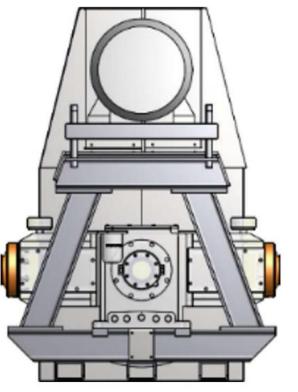




Prototype design – mechanical compressor

Design of a complete compressor prototype for laboratory use

- New proprietary low-noise hydraulic relief valve developed
- Development of supporting balance-of-plant components
- Compressor power-frame developed integrating all submodules:
 - Compressor head
 - Crank-case,
 - Electrical motor
 - Supporting balance of plant components



Compressor power-frame

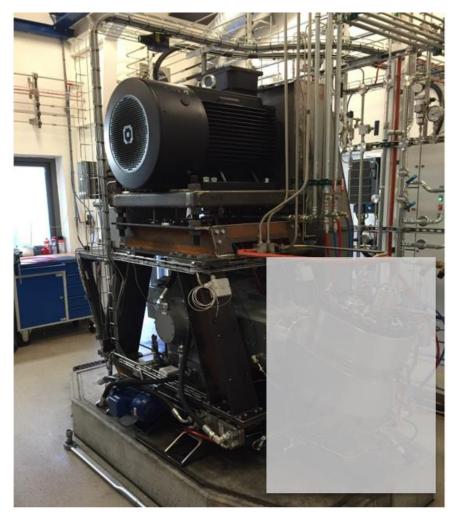




Laboratory testing – mechanical compressor

Extensive laboratory testing of the MC prototype at NEL in Denmark

- More than 4000 hours of tests performed
- Cold and hot tests from -10degC to +50degC
- Capacity tests with up to 60kg/hour demonstrated
- Energy tests: Validated reaching of the targeted 1,18 kWh/kg
- Endurance tests: achieved 100 million cycles diaphragm lifetime
- Noise tests: confirmed ability to reach <60dB in a HRS setting



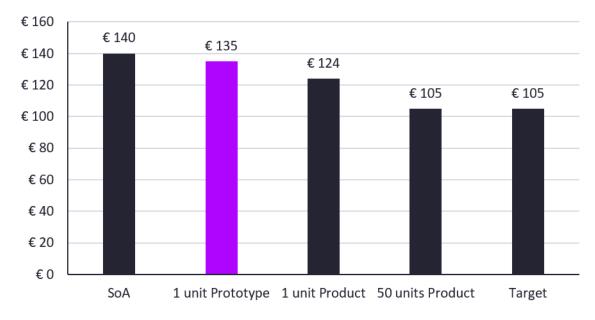




Cost reduction assessments – mechanical compressor

Pathway identified to achie €105/kg/day target

- Experienced cost on Prototype, already 3,6% cheaper than SoA (commercial industrial compressor in volume manufacturing)
- 1st unit of product design expected to reduce costs with further 7,4% due to lower labor costs (design optimized for assembly)
- 50 unit/year volume manufacturing to further lower costs with 16%, due to both lower labor and components costs



€/kg/day CAPEX - Mechanical Compressor





Final Event Building up a metal hydride compressor prototype pt. 1 - MAHYTEC

Speakers Jean-Michel TISSERAND Mathilde BANGOURA

Event Final Event, 24/02/2021

Location On-line

0 108 H2

Innovative compression solutions for efficient hydrogen mobility



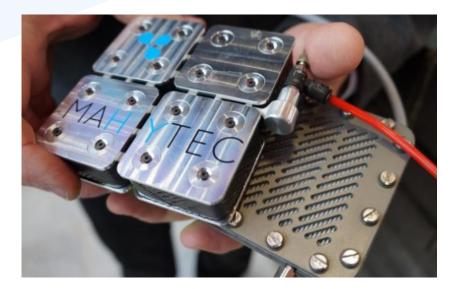


02/24/2021 | COSMHYC Final Event Presentations

Hydride application

Hydride tank can be used to store small or large amount of hydrogen for various applications.

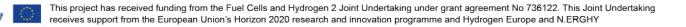
- Small fuel cell vehicle
- Electricity generator











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Metal hydride reactor

A metal hydride reactor is composed of:

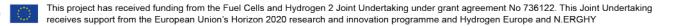
- Metal hydride
- A shell

-









Selection of adapted metal hydride

Hydride selection for compression application

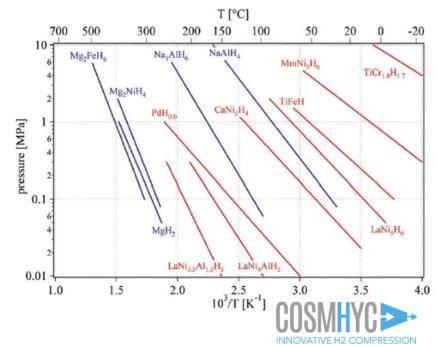


For hydrogen storage, a perfect hydride would stay at the same pressure when temperature increases.

For hydrogen compression, a perfect hydride would increase grandly its pressure with a small temperature increase.

Pressure and temperature are not the only parameters.

- To perform well over the time: cyclic stability, impurity
- To be competitive over other technology: H-Capacity and cost
- · To be efficient: thermal capacity, thermal conductivity, enthalpy



02/24/2021 I COSMHYC Final Event Presentations

Selection of adapted metal hydride

Environmental impact

Most alloys implemented in competitors compressor use rare earths.

Rare earths hydride are well known, offer good performance and ease of activation but...

We chose not to use rare-earths because:

- They are expensive
- Extraction and purification process \rightarrow pollution
- Can be subject to commercial limitation







Selection of adapted metal hydride

Hydride combination

. . .

The compression ratio of an hydride will depend on its own characteristics and on the temperature range.

If compression ratio isn't large enough to reach the desire pressure, hydride can be cascade.

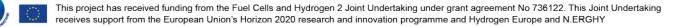
First stage will compress hydrogen from H2 source to the second stage input. Second stage will compress hydrogen for the third stage

Final stage will reach the desire pressure

Overlapping is an important parameter for hydrides selection

Hydride	Pressure (bara)												
	0				20				100				500
A1													
A2													
A3													





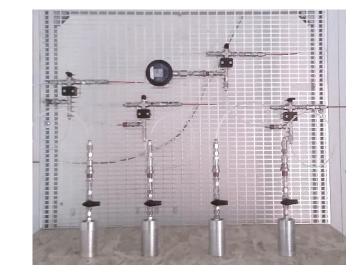
Selection of adapted metal hydride

Hydride test

For each parameter, tests such as PCT, cycling test, kinetics, compression... need to be performed by manufacturer.

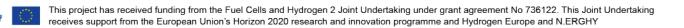
Hydride selection requires a huge amount of work and time







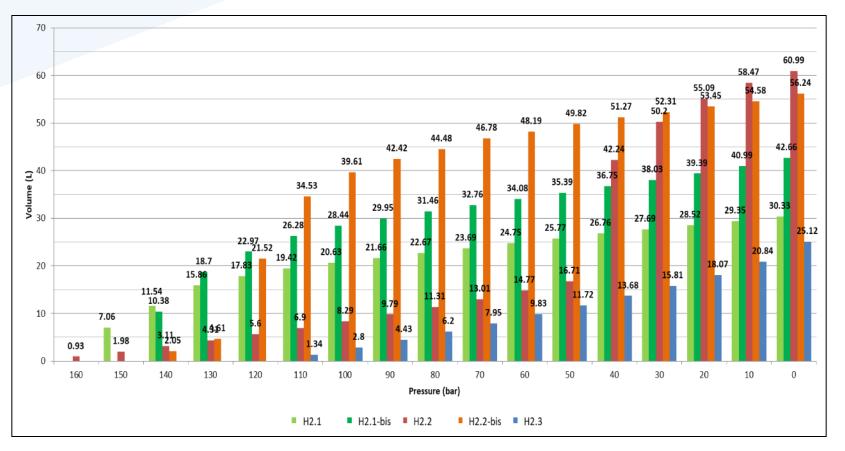




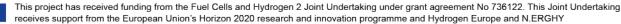
Selection of adapted metal hydride

Preselected hydride comparison

Some hydride will reach higher pressure, but with an average capacity. Other will reach a better capacity but compress at a lower pressure And some will just be... bad

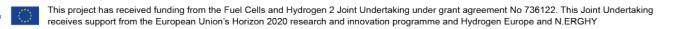






Hydride manufacturing



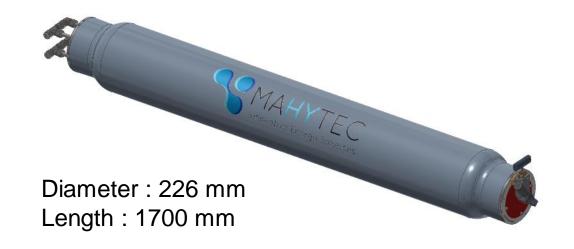


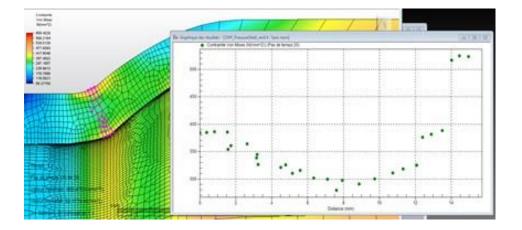
Reactor design

Shell

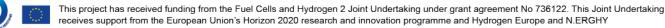
Compressor shells are complex due to many constrains:

- Safety: the shell needs to withstand pressure up to 450 bar.
- Temperature: the reactor will operate up to 180°C.
- Weight: low thermal inertia.
- Be Price-competitive
- Compatibility with hydrogen









Reactor design

Heat exchanger

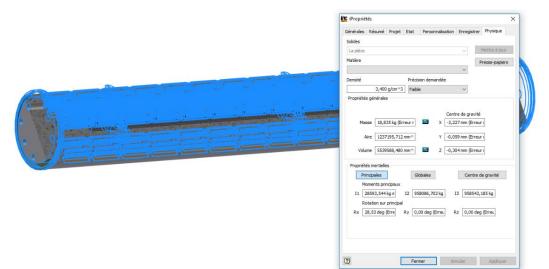
Heat exchangers have huge impact on system efficiency. Reducing cycling time by 50% will increase H2 flow by 2

But heat exchanger complexity is alike to its importance. It must :

- Reduce distance between powder and heat exchanger
- Fast heating/cooling property
- Resistance to the pressure
- Hydrogen compatibility
- Hydride expansion (compartmentation)
- No poisoning of the hydride
- Working from -40 to 180°C
- Have Low thermal inertia
- Be Easily filled
- Be Compact

. . .

• Be Price-competitive





Reactor approval

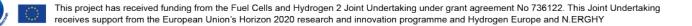
Approval

As compressors are pressured devices, all stages have been tested and approved according to DESP 2014/68/UE

- Hydrogen compressor
- Serial number of the tank: CMY200-N-000 or CMY440-N-000
- Test date: AAAA/MM
- Test pressure (PT): 644barg
- Maximum filling pressure: 20barg or 100barg
- Minimum filling temperature: +10°C
- Pressure min/max : -1barg/200barg or -1barg/440barg
- Operating temperature: -40°C/180°C
- Service temperature: +10°C/160°C
- Hydrogen only: Group 1 fluid
- Valve pressure: 200barg or 440barg



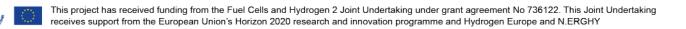




(FCH)







Final Event Building up a metal hydride compressor prototype pt. 2 - EIFER

Speaker Rami CHAHROURI

Event Final Event, 24/02/2021

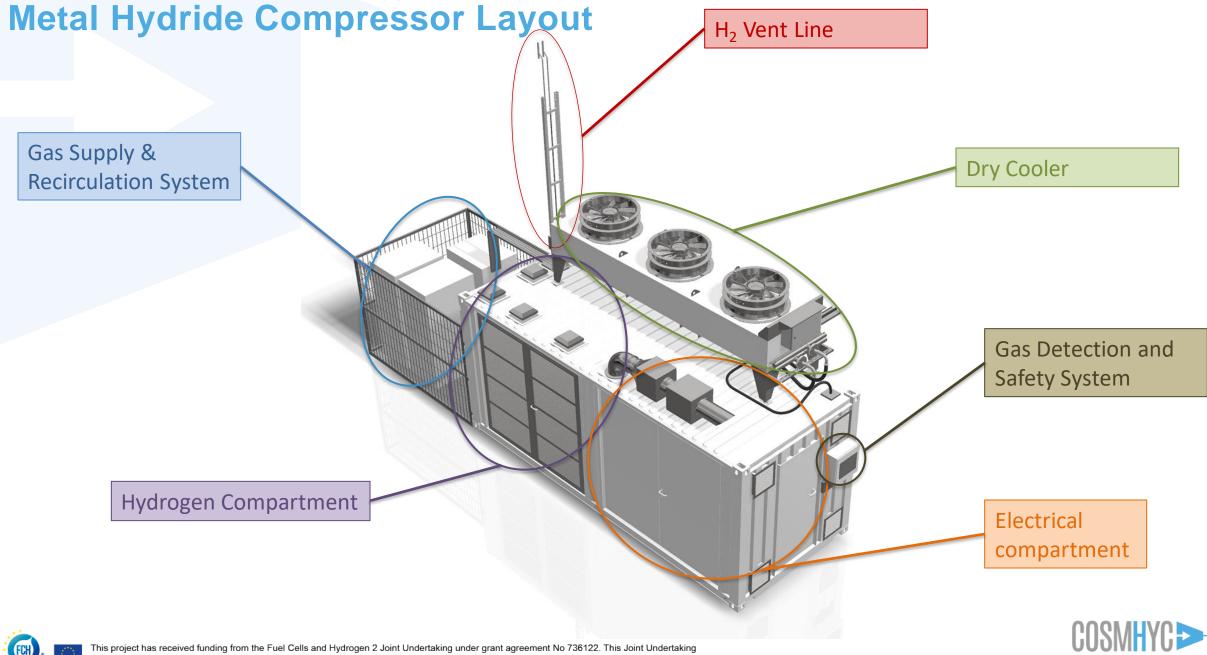
Location On-line

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Innovative compression solutions for efficient hydrogen mobility



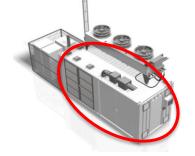




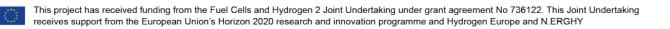
receives support from the European Union's Horizon 2020 research and innovation programme and Hydrogen Europe and N.ERGHY

Container Delivery









Hydrogen Compartment









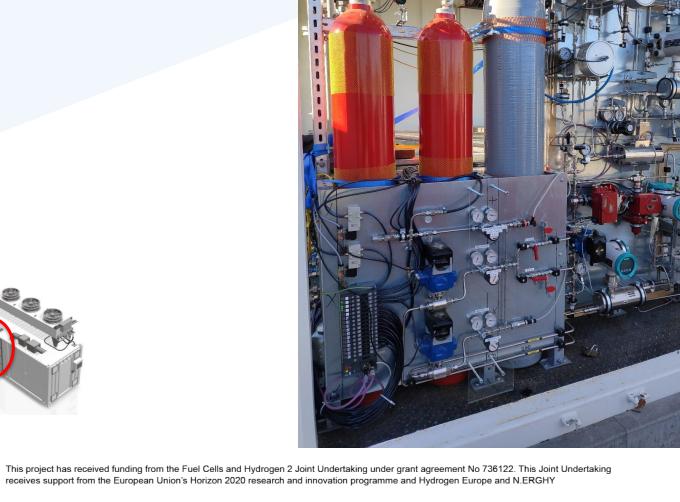


Hydrogen Valve Panel









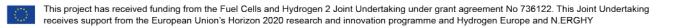
Electrical Compartment











Gas Detection & Safety System

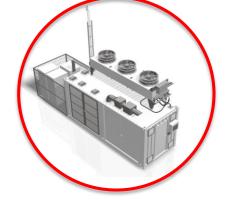






MHC Compressor







24th of February 2021

Tests and results of the COSMHYC compressors

Speaker David Colomar EIFER



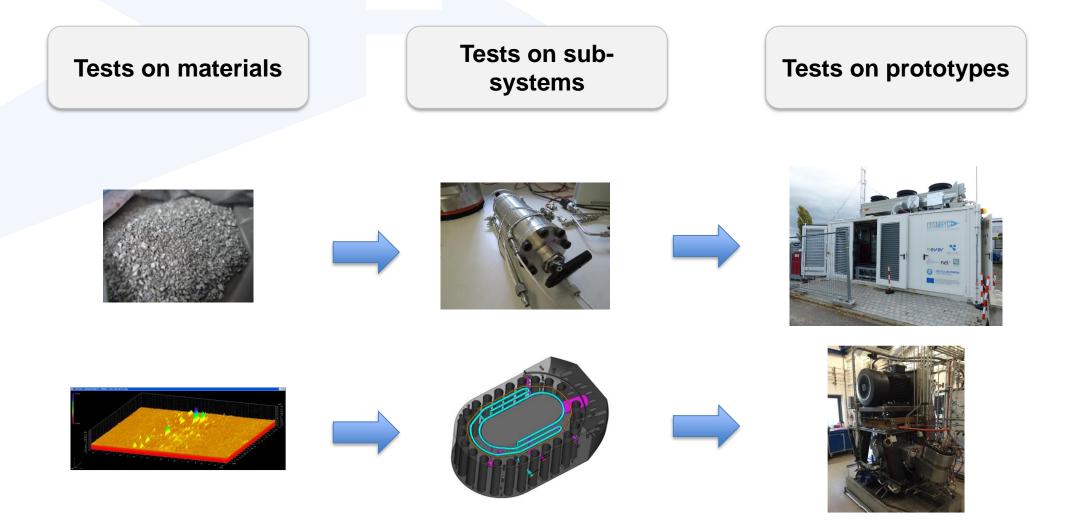
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Innovative compression solutions for efficient hydrogen mobility





Different tests were performed along the project

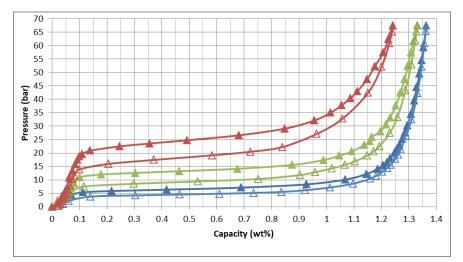






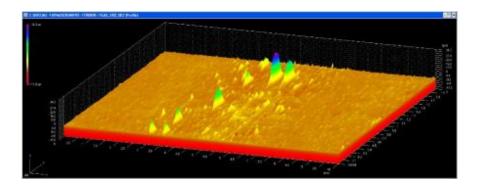
Testing on materials : new hydrides and membrane materials

- \Rightarrow Tests performed on 11 different rare earths free hydrides
- PCT curves, to determine compressor capacity and relationship between temperature and pressure
- Main issues encountered: activation, contamination with impurities, heat exchange
- ⇒ Main result: Appropriate hydrides were identified for compression from 5 bar to 450 bar



\Rightarrow Investigating compressor membranes

- Assessing the impact of roughness on life time
- Proposing improvement strategies: surface treatment, new materials
- ⇒ Main results: several 10th of millions cycles demonstrated without failure







Testing innovative subsystems: metal hydride tanks

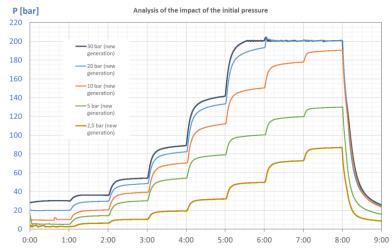
⇒ Different tank concepts were developed and tested

- Increasing mechanical resistance while reducing thermal inertia
- Optimising capacity while enabling a good reaction kinetics
- Reaching appropriate flow rates and compression ratios
- Validating at representative scale the performances expected at material level

\Rightarrow Main results:

- Performances at material level confirmed
- Exponential increase in P with growing T: an expected challenge for optimization
- Compression ratios of 10 to 35 demonstrated for 1 stage !





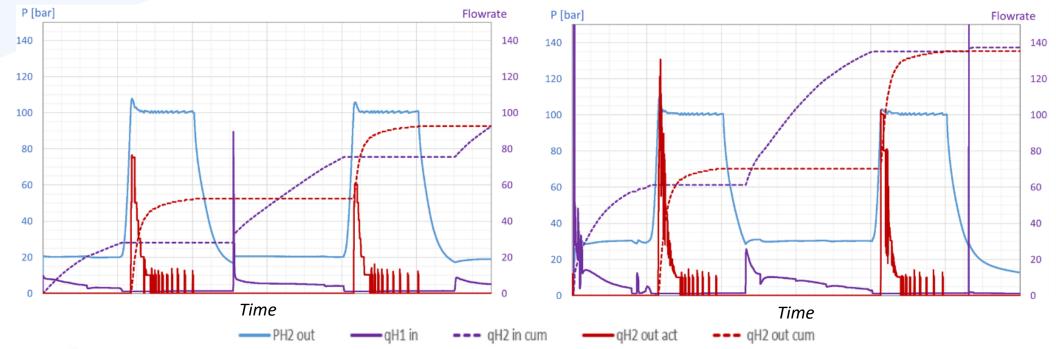




Testing innovative subsystems: metal hydride tanks

⇒ Lessons learnt from tank behaviour

- Significant impact of inlet pressure on desorption flow
- \Rightarrow Confirmation of the added value of pressurized H2 production
- Desorption profile strongly inhomogeneous : 70% of the hydrogen desorbed in 25% of the time
- \Rightarrow Important role of the control strategy : identifying the techno-economic optimal desorption time

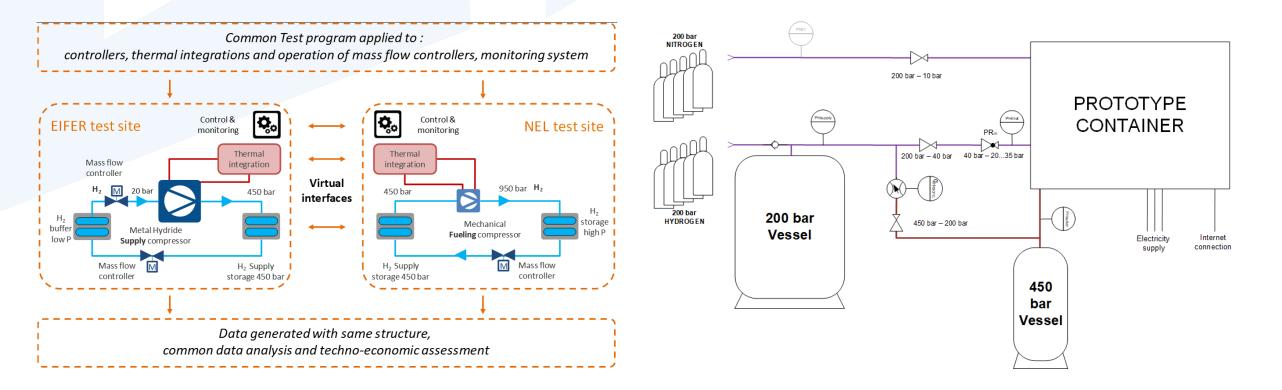






Testing prototypes: testing concepts

⇒ Both prototypes tested on separated sites to facilitate monitoring and maintenance







Testing prototypes: the mechanical compressor

- ⇒ The mechanical compressor prototype was tested in Denmark at NEL facility
- More than 4000 h of tests were performed, including:
- Cold and hot tests : operation from -10° to +50°C successfully demonstrated
- Capacity tests : capacity of more than 60 kg/h demonstrated
- Pressure inlet/outlet well in phase with the capacity of the metal hydrde compressor
- Energy tests : consumption significantly improved compared to state-of-art
- Endurance tests : 10th of millions of cycles demonstrated without failures, more than 5000 starts and stops





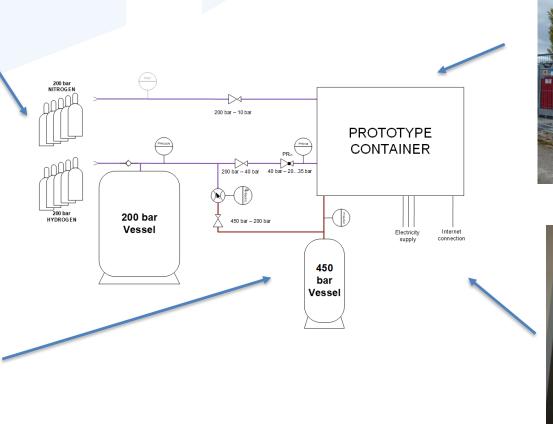




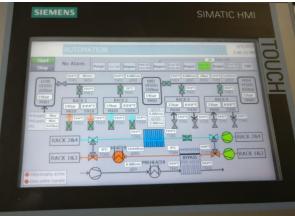
-10 °C compressor testing















\Rightarrow Operation and maintenance issues

- Surprisingly few problems encountered with the core technology as long as the purity level of hydrogen matches the requirement
- Most issues encountered with the BOP, including:
 - Reliability of H2 components
 - Reliability of thermal BOP
 - Tightness of heating integration
 - Material compatibility of heating fluid with components











- \Rightarrow Pressure level reached stage 1: 28 bar -> 112 bar
- ⇒ Pressure level reached stage 2: 97 bar -> 429 bar
- Significantly higher pressures possible >450 bar, but not implemented in automatic mode for safety reasons
- A compression ratio of > 15 achieved
- < 50% useful time in the process: a strong potential for further optimization remains
- Further optimization needed in well-defining optimal intermediate pressure
- ⇒ Prototype as a stand-alone solution already today meets the requirements of several end users needs

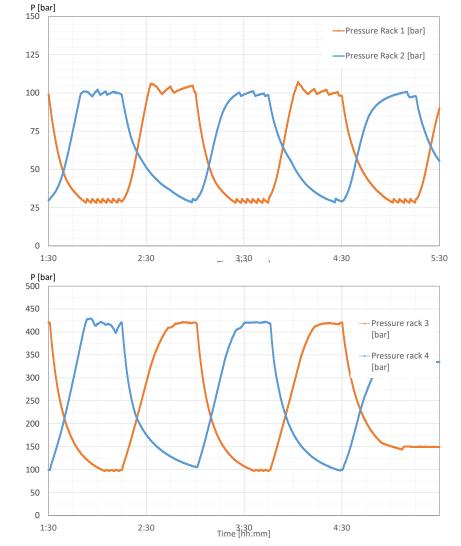
















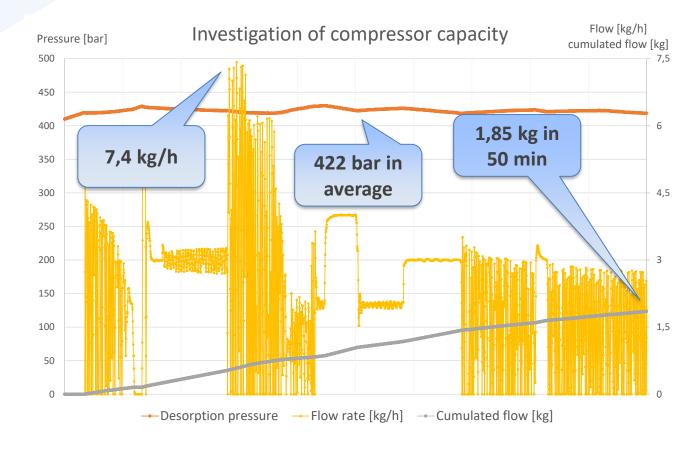
⇒ Capacity: target = 2 kg/h

- Peak flow rate observed : up to > 7 kg/h
- Flow rate over ~1h : 2,2 kg/h
- Average flow rate depending on:
 - Setting cycling time
 - Heat power profile
 - Set-up temperature
 - Outlet pressure
 - Climatic conditions
 - User profile
- Values observed currently vary between a few 100 g/h to several kg/h
- Further investigations still ongoing

\Rightarrow More than 10 X the state-of-art reached !







⇒ Energy consumption

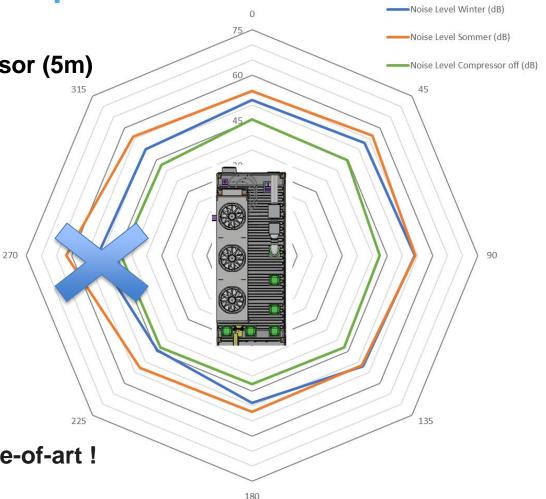
- Only preliminary analysis so far as additional tests still ongoing
- Energy consumption consists of :
 - Heating energy for absorption/desorption
 - Inertia of hydrides, tanks, thermal circuit
 - Electricity for auxiliaries
 - Electricity for cooling fans
- Preliminary values show a consumption significantly better than the state-of-art of hydride compression but higher than comparable mechanical compressors (> 9 kWh)
- However, if a waste heat source is available, electricity consumption can be lower than 1 kWh/kg
- Significant improvement potential : auxiliaries, thermal insulation, inertia of tanks etc.

⇒ Strong potential for using the technology where waste heat (industry, H2 production) is available





- \Rightarrow Noise disturbance were investigated around the compressor (5m)
- 2 typical operation modes were assessed:
- Summer / day mode, with the cooler at maximal working power.
- Winter / night mode, with the cooler at a lower speed.
- In average, the following noise source was measured:
- 53,9 dB in summer / day mode
- 50,6 dB in winter / night mode
- The main noise source is the ventilation,
- This could be mutualised with other HRS equipment
- This noise source is qualitatively less disturbing than a piston
- \Rightarrow The overall noise disturbance is much lower than the state-of-art !







Overall conclusions

- \Rightarrow 2 technologies developed and prove their complementarities
- ⇒ Scale-up successfully achieved
- \Rightarrow TRL level successfully increased
- ⇒ Pressure targets achieved
- \Rightarrow Strong potential for noise reduction demonstrated
- ⇒ Further optimization is still needed, especially regarding energy consumption (when no waste heat is available), reliability of BOP, flow rate management
- ⇒ Activities continue within COSMHYC XL & COSMHYC DEMO, towards demonstration and commercialization





Thank you for your attention !

Contact: colomar@eifer.org







24th of February 2021

Techno-economic assessment

Speaker Jan Zerhusen



ludwig bölkow systemtechnik



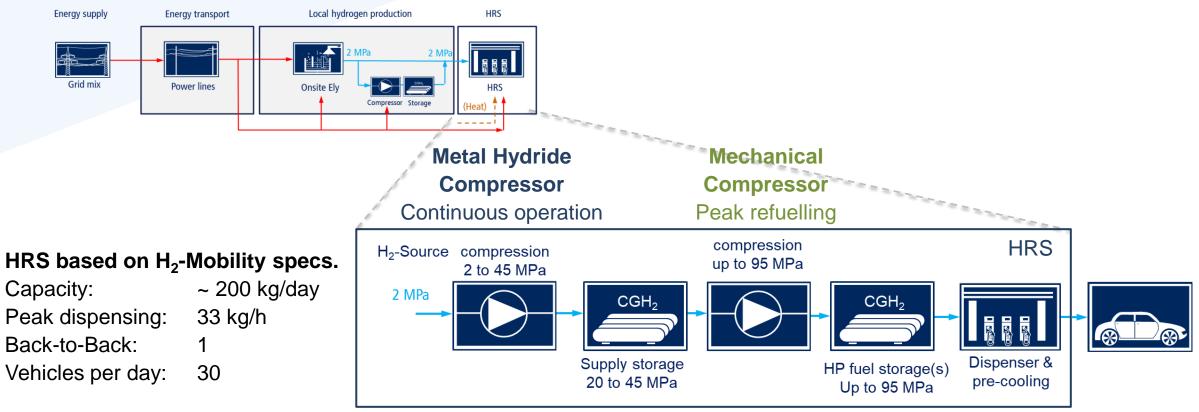
Innovative compression solutions for efficient hydrogen mobility





Cost assessment 70 MPa hydrogen refuelling station (HRS)

Hydrogen supply scenario: Lowest input pressure 2 MPa (e.g. from local LP-storage) Hybrid compressor concept: Continuous operation of metal hydride compressor and peak operation of mechanical compressor

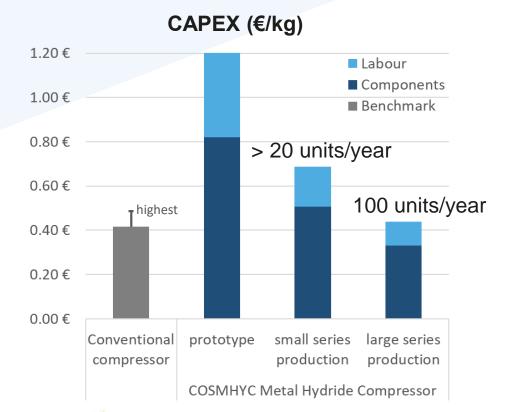






Cost assessment Metal Hydride Compressor

CAPEX: reduction due to series production \rightarrow reduced complexity, improved assembly, higher purchase volume, etc. CAPEX: metal hydride compressor on par with benchmark \rightarrow metal hydride advantage in some cases OPEX: cost advantage for metal hydride \rightarrow heat usually less expensive than electricity



1.20 € 1.00 € 0.80 € 0.60 € 0.40 € 0.20 € - € Conventional compressor prototype small series large series production production [E]

OPEX (€/kg)

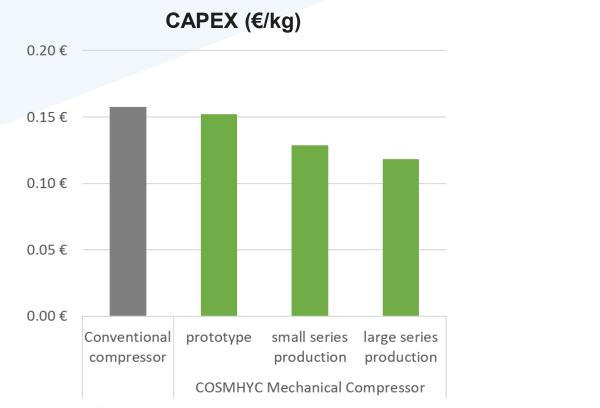
Electricity: 0.15 €/kWh Heat: 0.03 €/kWh

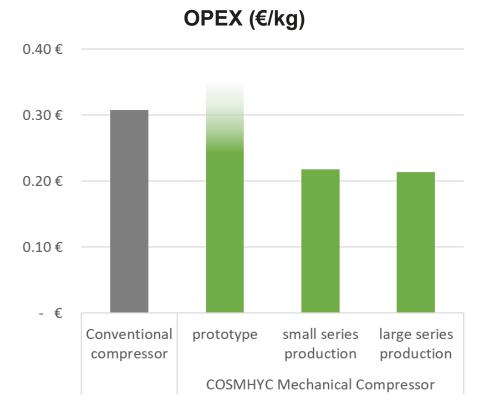




Cost assessment Mechanical Compressor

CAPEX: Material costs of prototype already below benchmark; further reduction when optimizing for series prod. OPEX: Reduced electricity consumption and increased lifetime compared to benchmark



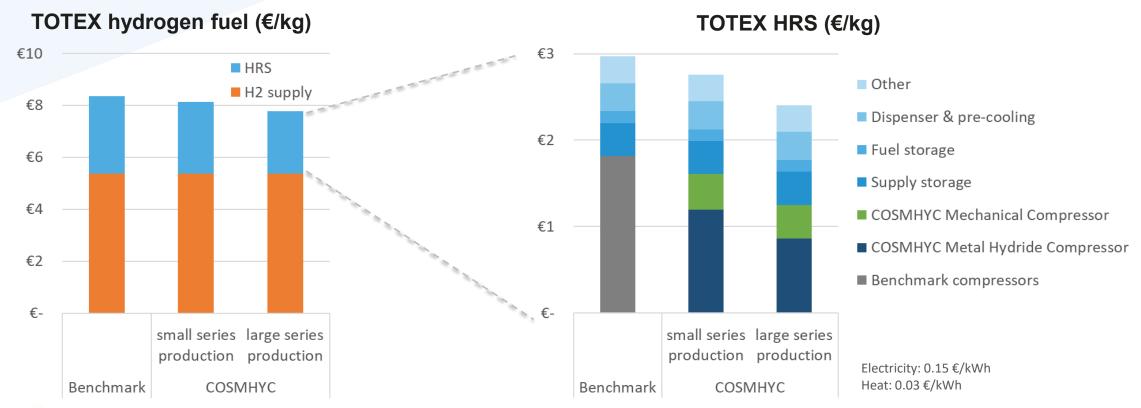






Cost assessment Total hydrogen costs

Overall cost savings at HRS of about 0.2 to 0.6 €/kg depending on mass production status Cost advantage also depends on electricity and heat costs

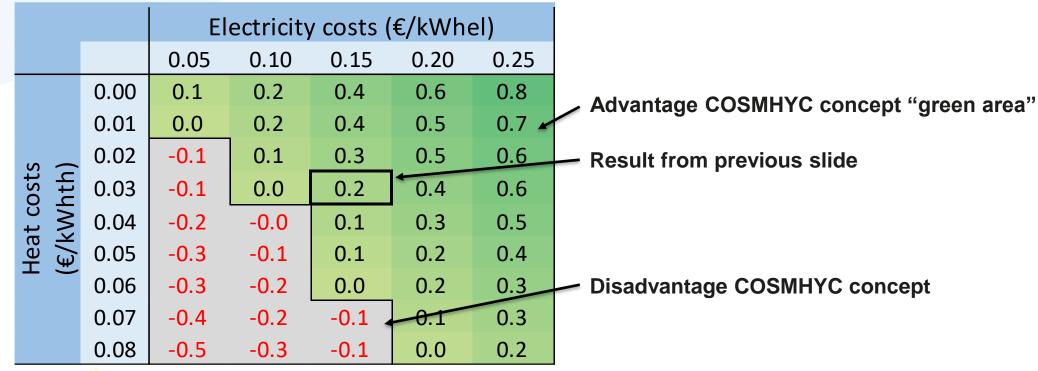






Cost assessment Impact of energy prices

Cost advantage of hybrid concept at small-series production Large-scale production extends "green area" to bottom left



Cost advantage (€/kg)





Cost assessment Conclusion

Cost advantage of COSMHYC compression concept expected based on project results and learnings

- Further development towards mass production required (End of project: TRL 5)
- Identified system simplifications etc. enable significant reduction of CAPEX compared to prototype
- At mass production, hybrid concept will be on par in CAPEX but will show lower OPEX compared to benchmark technology
- Cost advantage over benchmark technology at moderate energy prices and HRS utilization





24.02.2021 I COSMHYC Final Event LBST analysis based on consortium inputs

Thank you for your attention!



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